
Control of *Thiothrix* bulking in a full-scale treatment plant with a sludge granulation strategy

Olivier Henriet

January 25, 2018

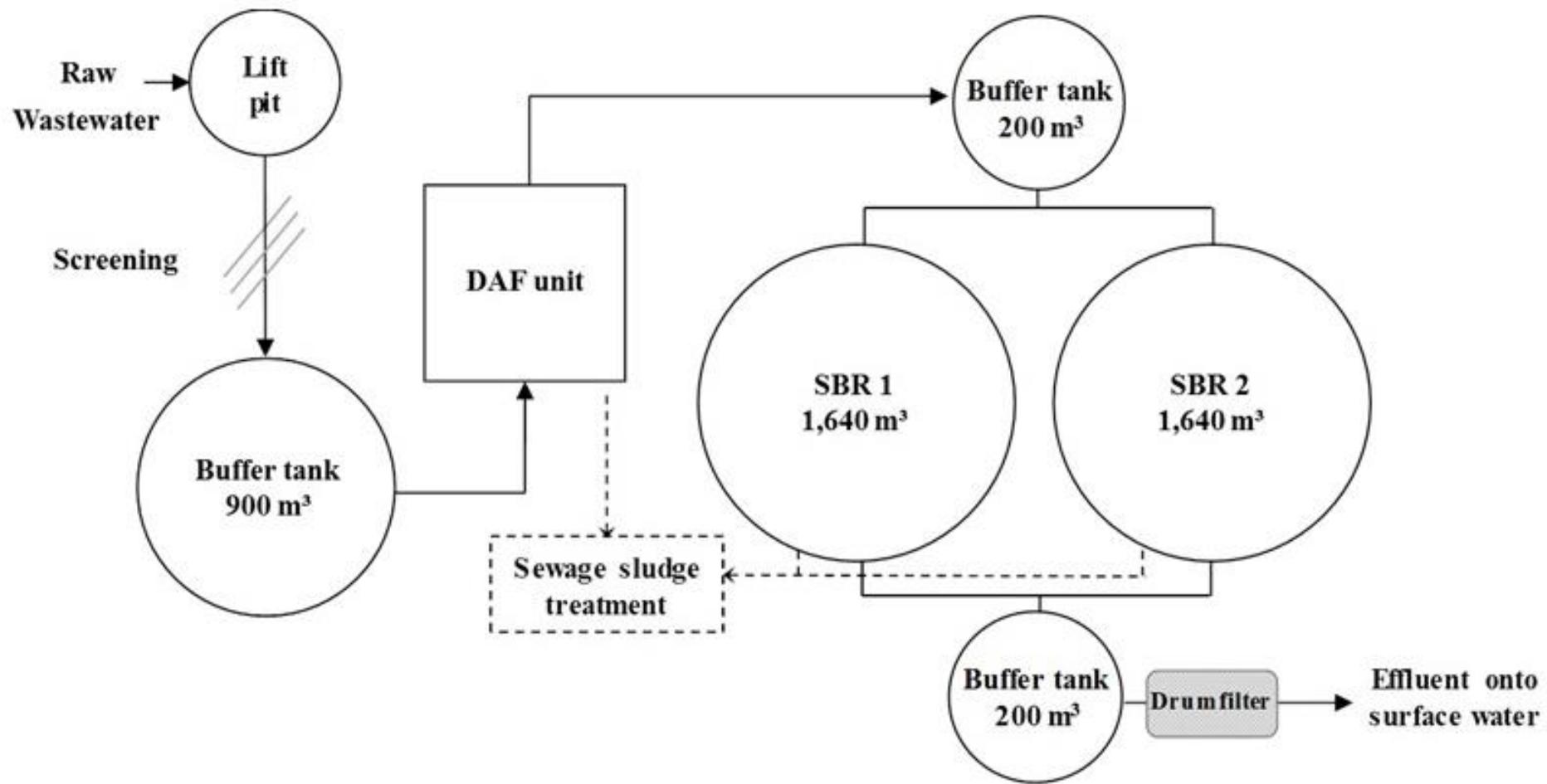
Dairy industry

Products

Milk
Cream
Ice Cream
Butter
Cheese
Yoghourt
Cookies



Full-scale plant



Henriet *et al.* 2017 *Sci. Rep.*

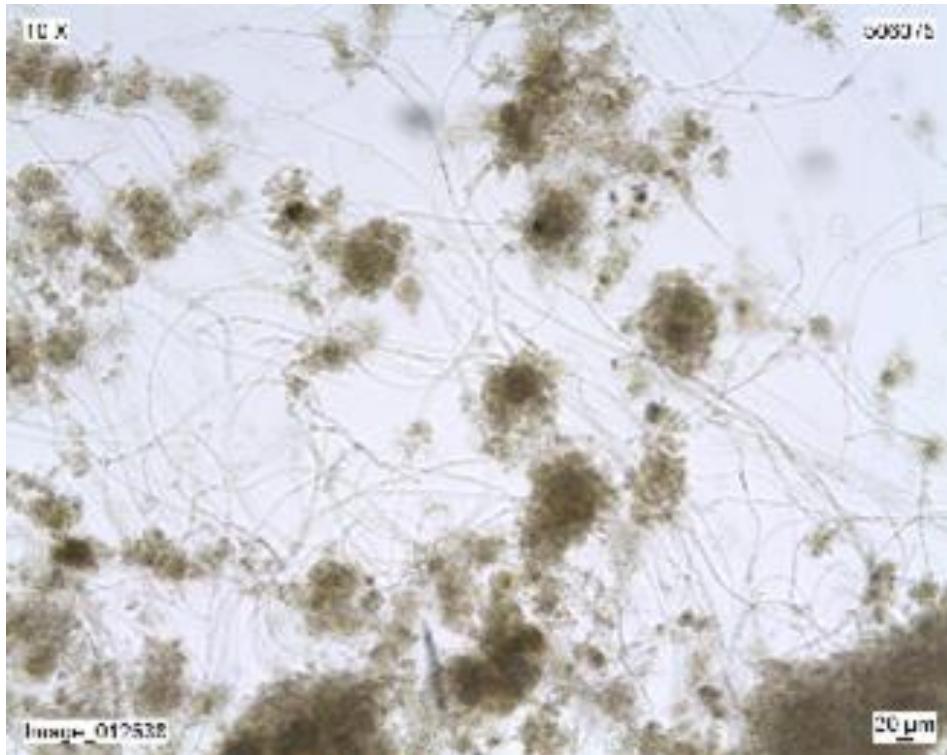
Full-scale plant



Pre-treated wastewater composition

Parameter	Mean (\pm SD)	Effluent discharge limits	Unit
Flow	870 (\pm 255)	-	$\text{m}^3 \text{ day}^{-1}$
Total COD	1358 (\pm 485)	110	mg L^{-1}
Soluble COD	868 (\pm 447)	-	mg L^{-1}
Total Nitrogen	55 (\pm 5)	15	mg L^{-1}
Total Phosphorus	11 (\pm 5)	2	mg L^{-1}
NH_4^+ -N (dissolved)	9 (\pm 13)	10	mg L^{-1}
TSS	-	30	mg L^{-1}
Temperature	24 (\pm 3)	-	$^{\circ}\text{C}$
pH	7.6 (\pm 0.2)	-	-

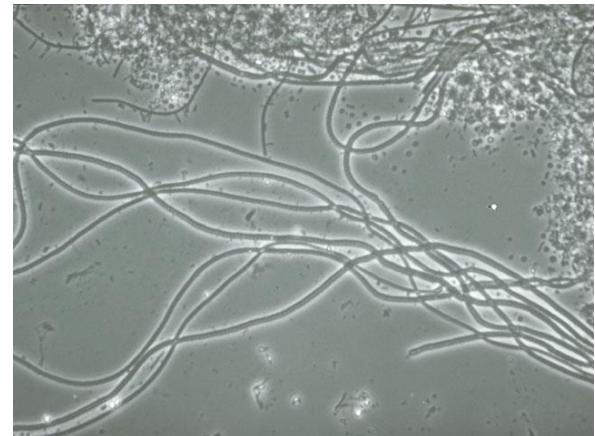
Filamentous bulking caused by *Thiotrix*



Thiotrix

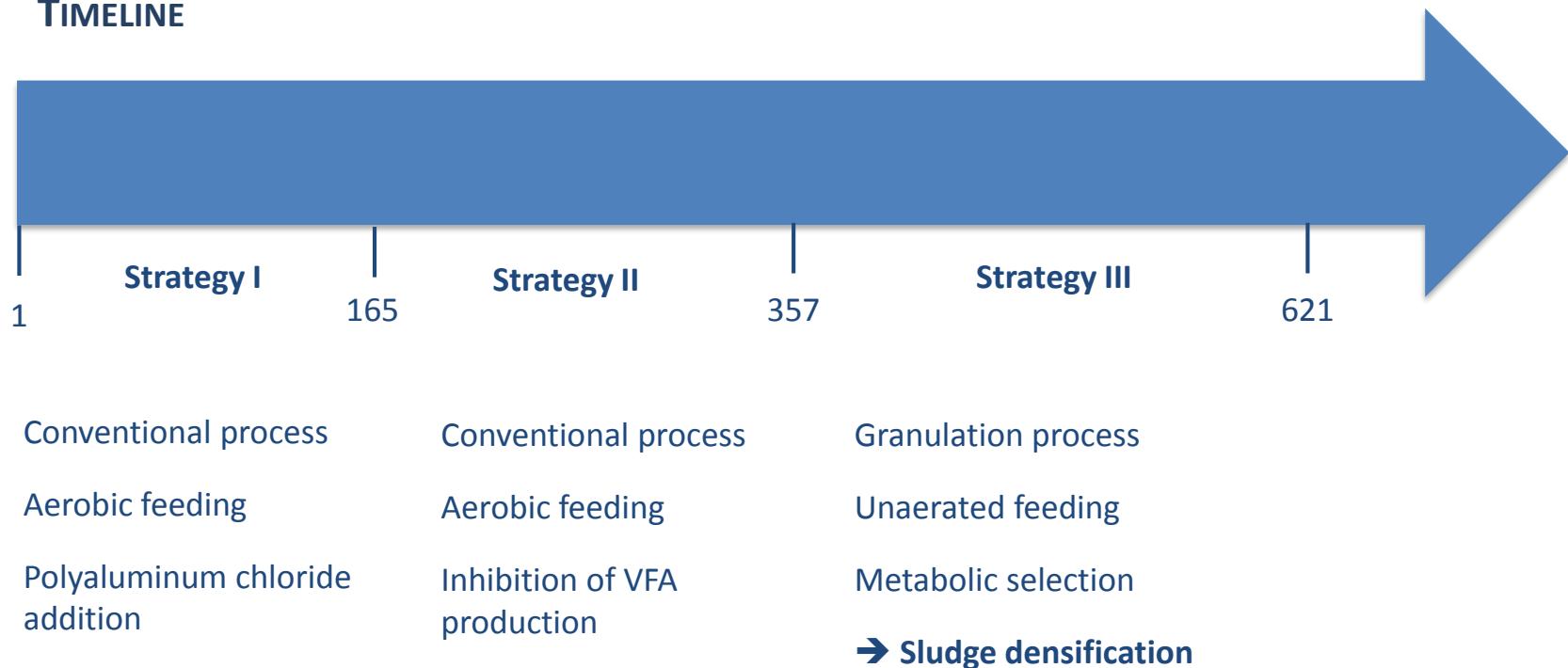
Abundance up to 70%

Recurring problem



Treatment strategies

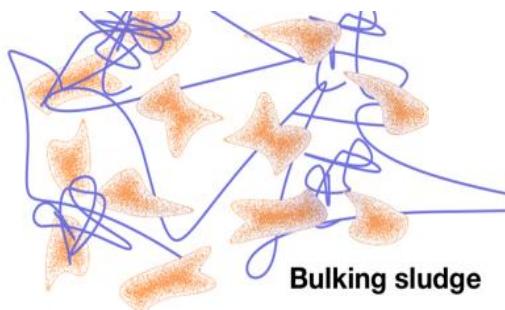
TIMELINE



Create a competition for the substrate

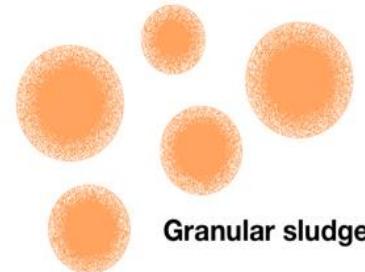
Acetate
Propionate

Aerated conditions



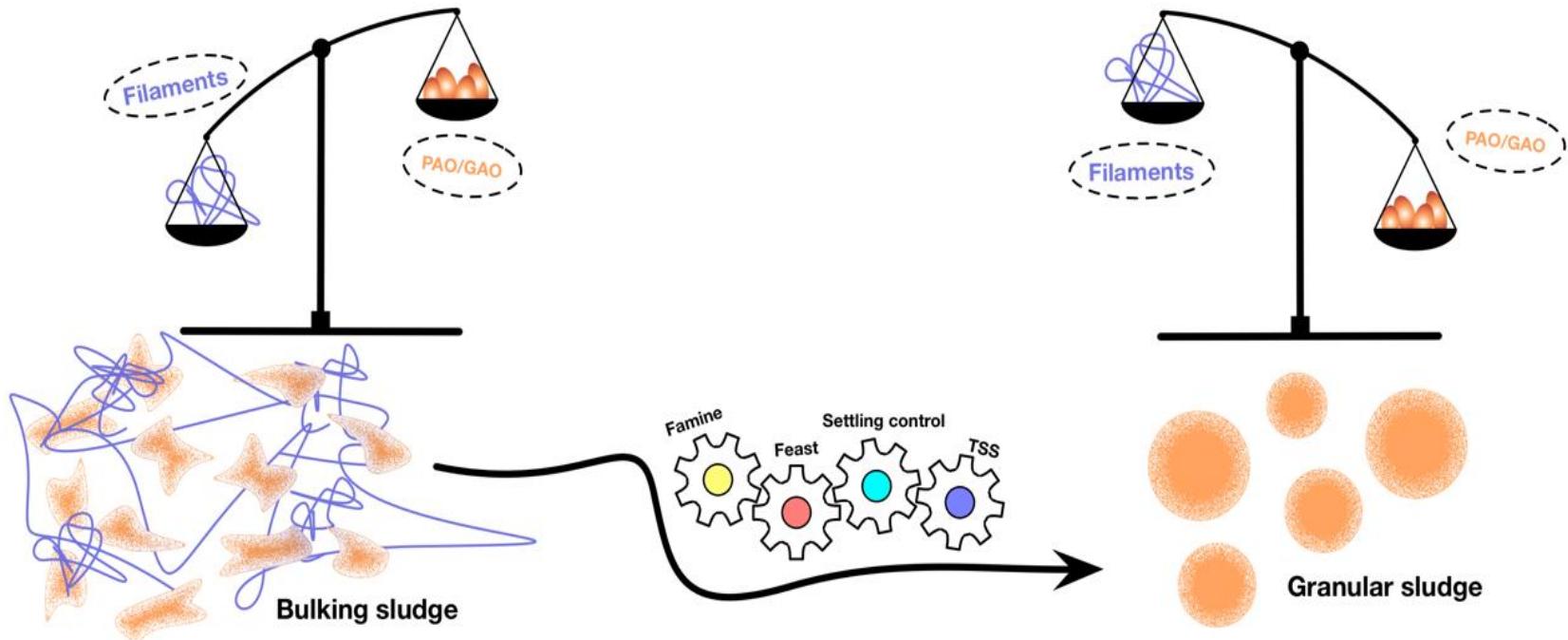
Filamentous bacteria

Non-aerated conditions



Biopolymer accumulating
bacteria

Create a competition for the substrate

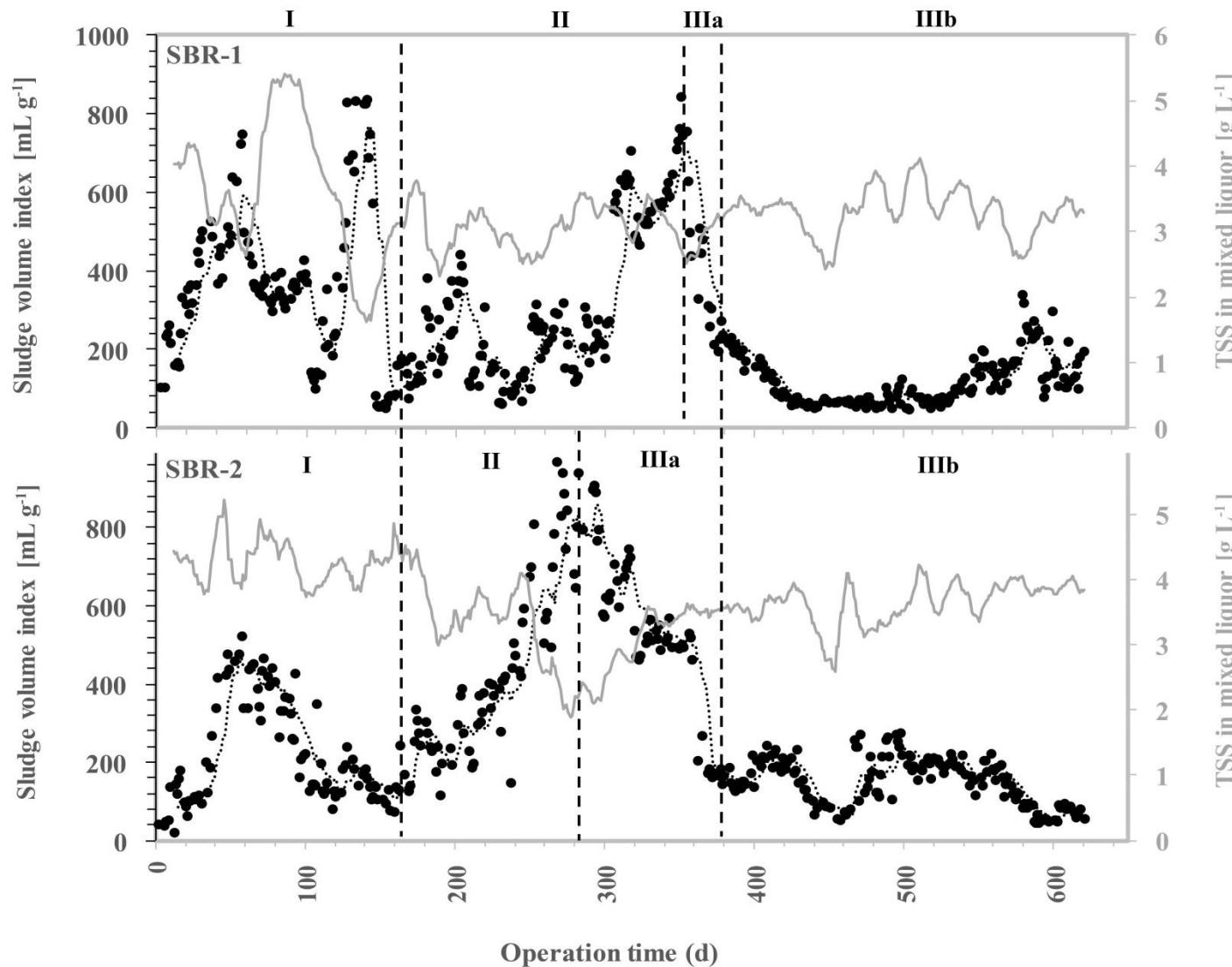


Meunier et al. 2016 *Bioresource Technol.*

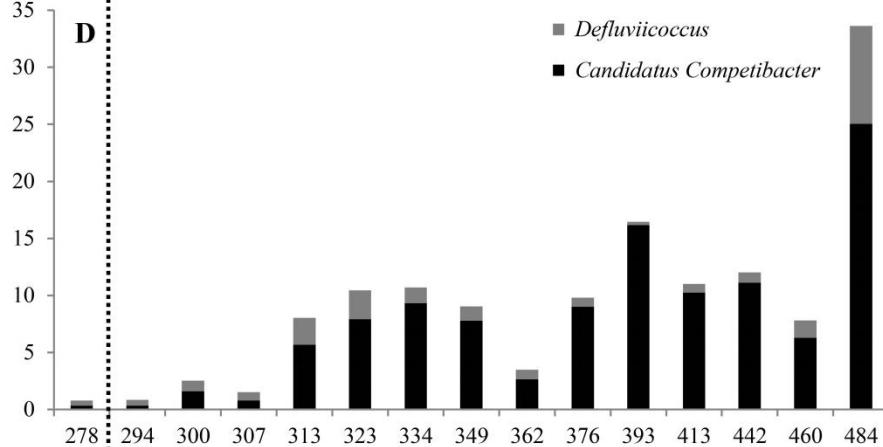
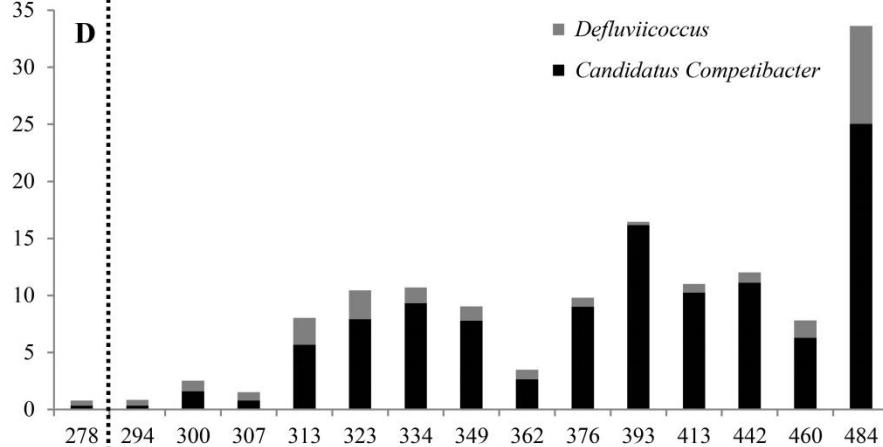
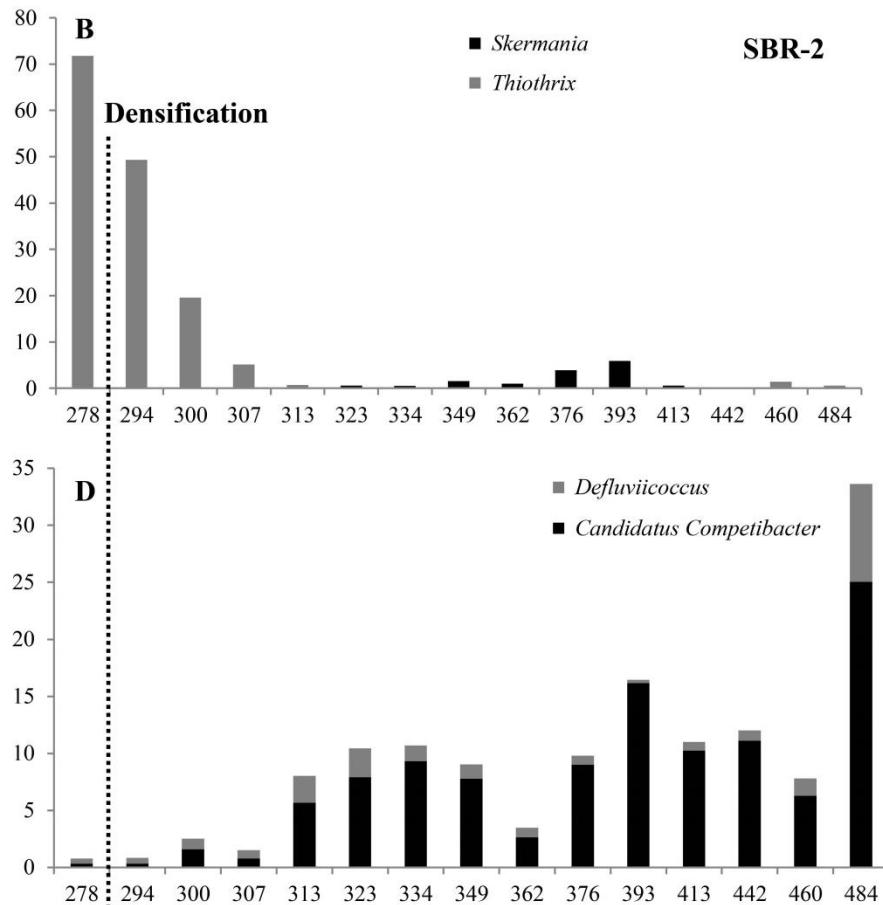
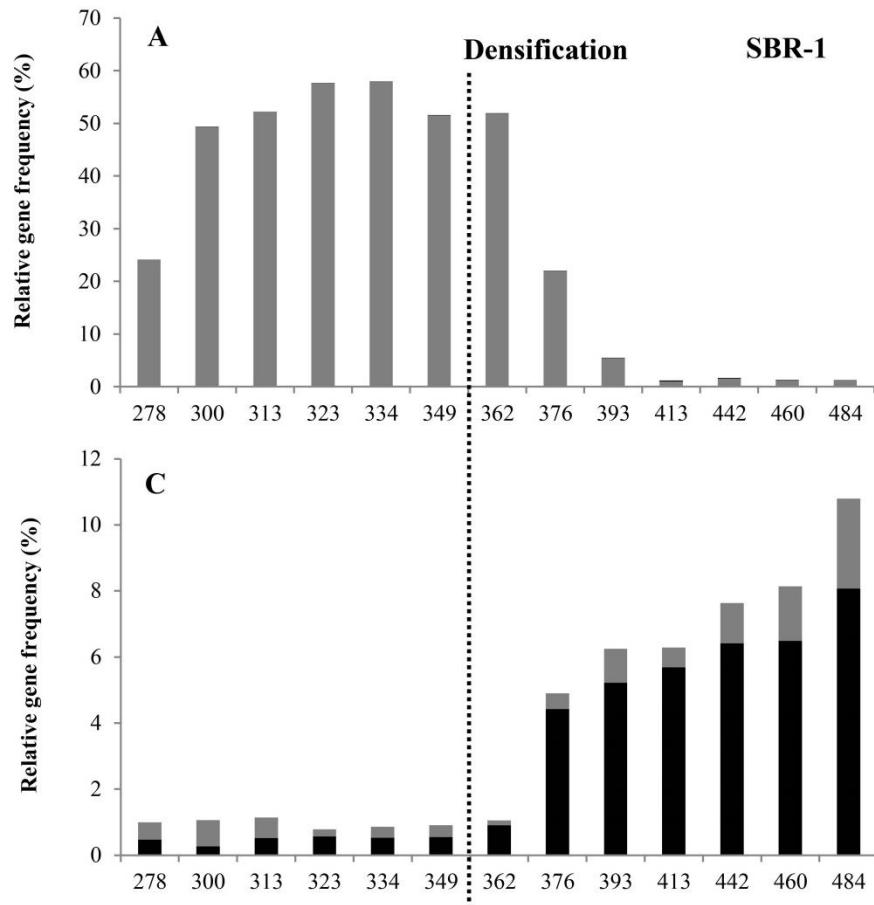
Operational parameters

SBR-1	Strategy	I	II	IIIa	IIIb
	Days	1-165	166-357	358-384	385-621
	Buffer tanks				
	Mixing with aeration	No	Yes	Yes	No
	Cycle				
	Aerobic feed	min	120		0
	Anaerobic feed	min	0		95
	Aeration	min	190		210
	Settling	min	50 - 60		40
	Decanting	min	110		115
	Sludge purge and idle	min	10		20
SBR-2	Strategy	I	II	IIIa	IIIb
	Days	1-165	166-282	283-384	385-621
	Buffer tanks				
	Mixing with aeration	No	Yes	Yes	No
	Cycle				
	Aerobic feed	min	120		0
	Anaerobic feed	min	0		95
	Aeration	min	190		210
	Settling	min	50 - 60		40
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	Sludge purge and idle	min	10		20

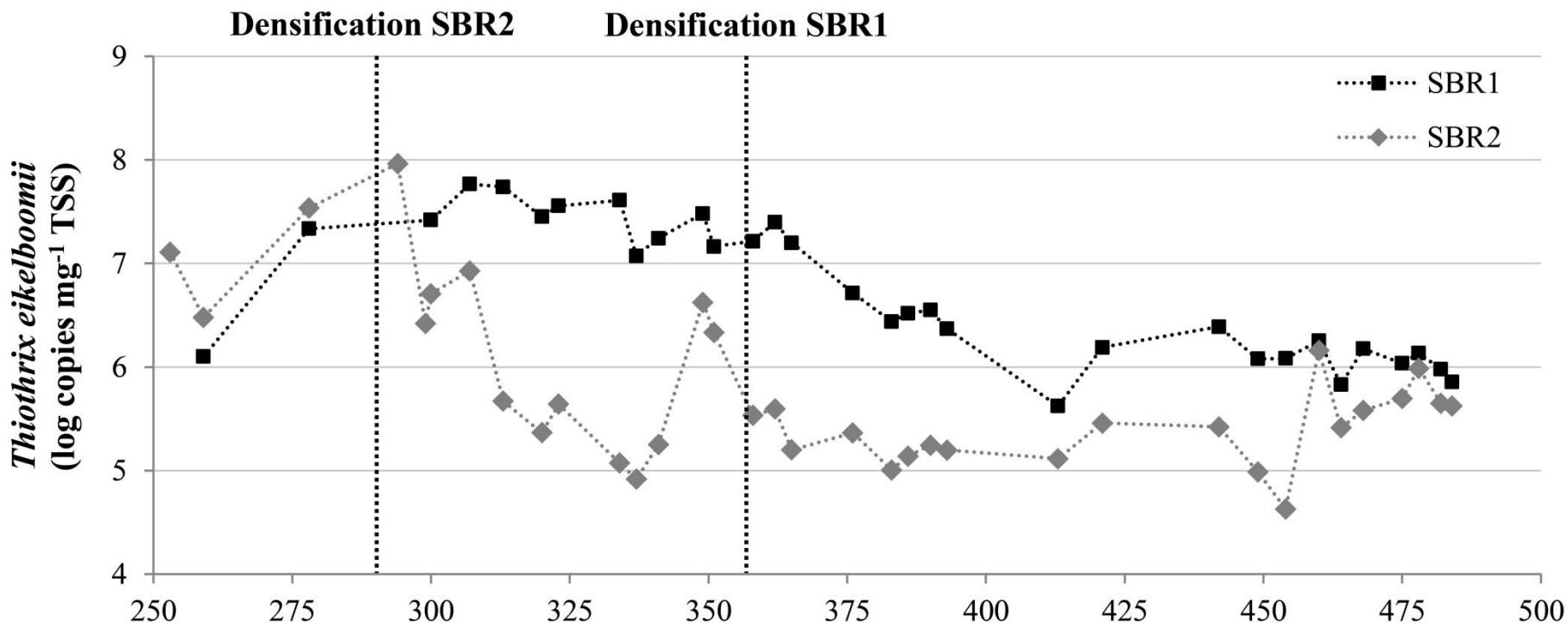
Sludge characteristics



Impacts on *Thiothrix* and accumulating bacteria



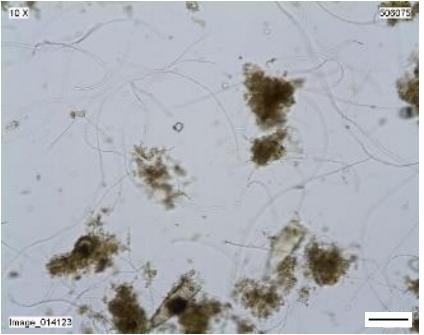
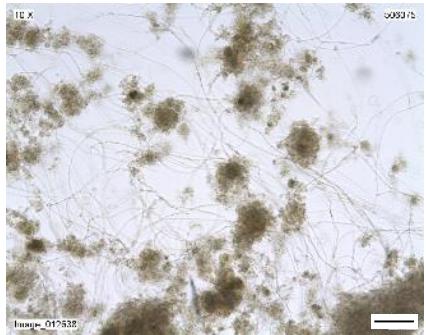
Impacts on *Thiothrix* and accumulating bacteria



Evolution of the sludge

SBR-1

I



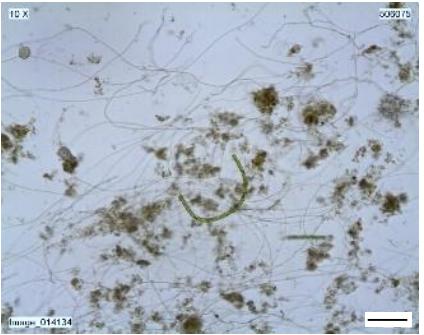
II



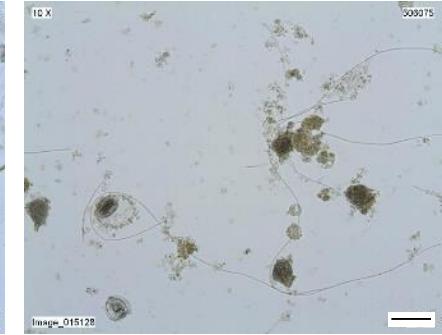
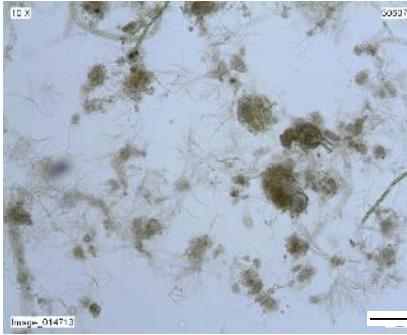
III

SBR-2

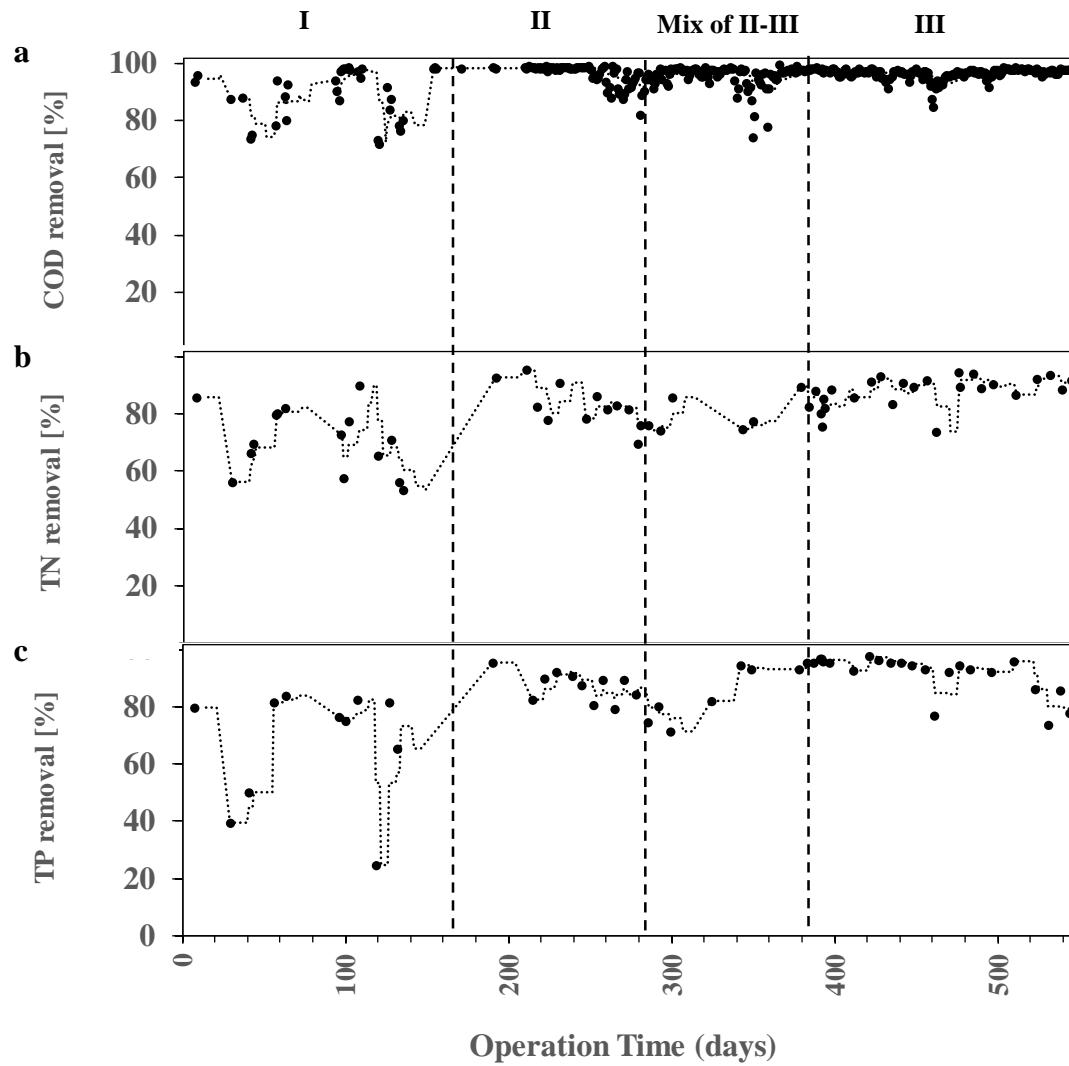
II



III



Performances of the plant



Comparison of operating parameters

Parameter	Unit	Conventional		Densification
		I	III	
Sludge retention time	d	24 - 37		29 - 54
Total suspended solids	kg m ⁻³	2.7 - 3.6		3.2 - 3.8
Sludge loading total	kg COD (kg TSS d) ⁻¹	0.150		0.102
Sludge loading biological	kg COD (kg TSS d) ⁻¹	0.232		0.233
Biological sludge production	kg DW (kg COD _{in WWTP}) ⁻¹	0.237		0.238
Volumetric load	m ³ (m ³ _{SBRS} d) ⁻¹	0.295		0.248
Specific energy demand for aeration	kwh (kg COD _{in bio}) ⁻¹	1.06		0.74

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Key messages

- **Filamentous bulking caused by VFA-consuming bacteria can be solved with a granulation strategy**
- **The metabolic selection is sufficient to form granules**
- **Aeration and settling time can be maintained at conventional values**
- **Granulation strategy reduces the energy demand**

Acknowledgements

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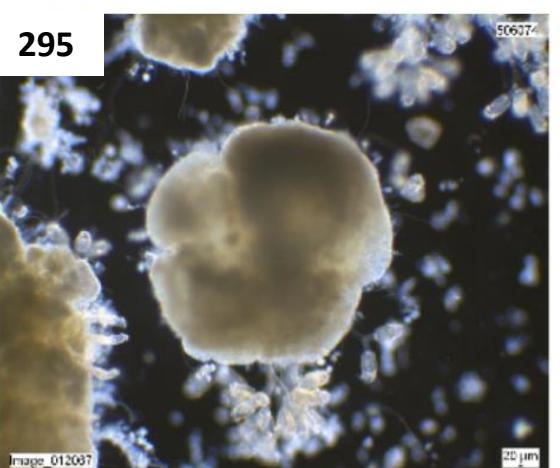
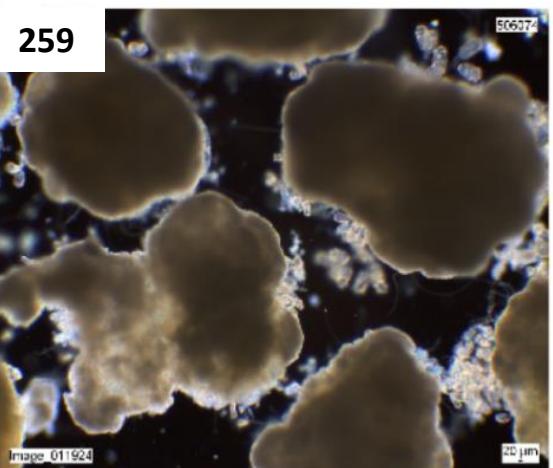
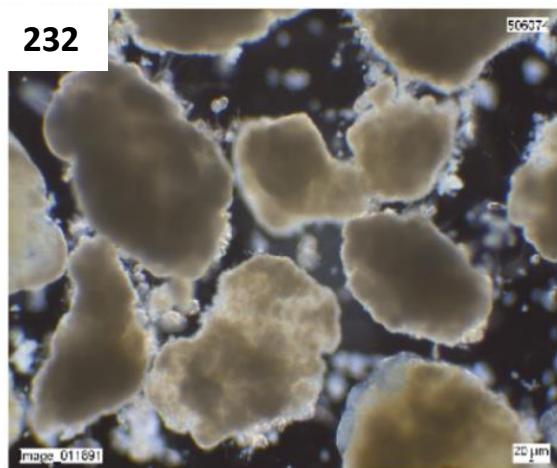
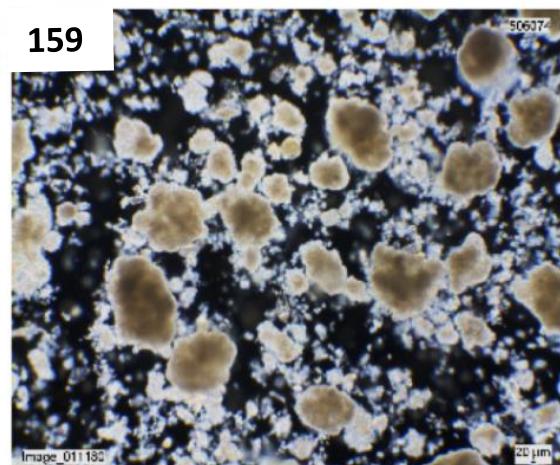
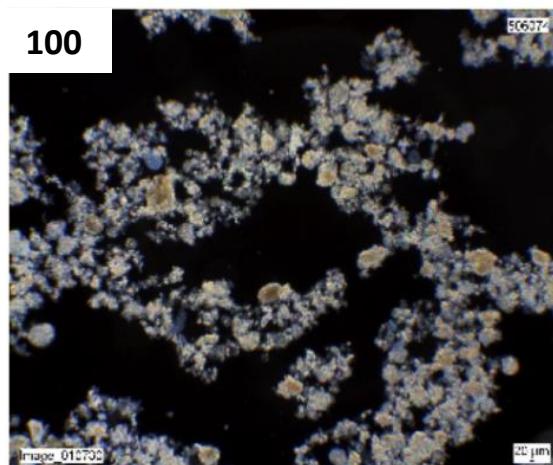
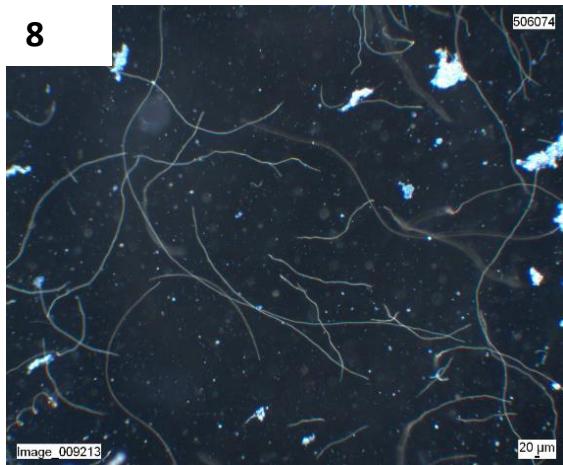
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January 25, 2018

Lab-scale assessment of the granulation strategy

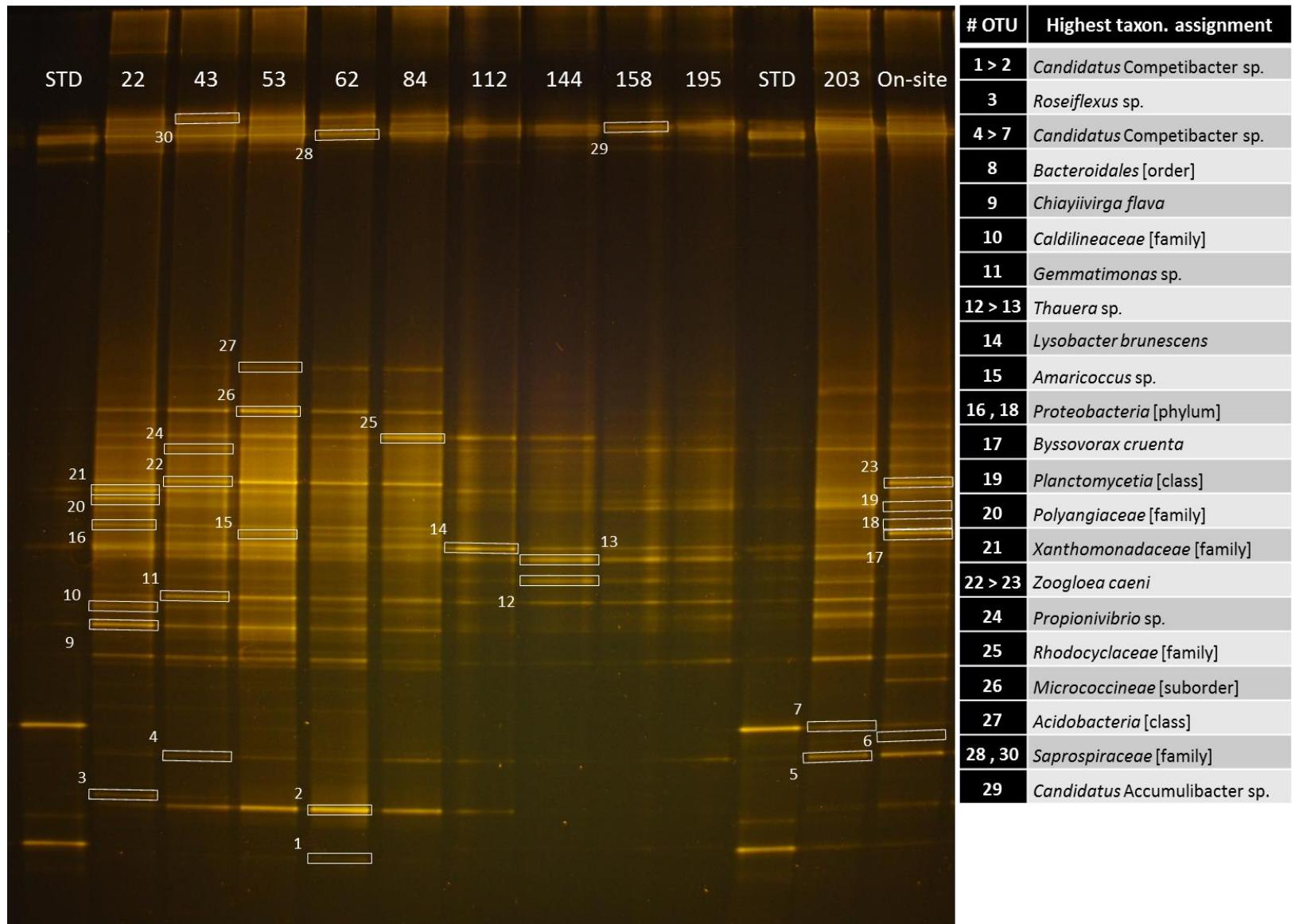
Periods	I	II	III	IV
Days	1-7	8-100	101 -160	161- 300
	Initiation	Storage metabolisms	Intensification	Maturation
<i>General characteristics</i>				
Volume exchange ratio	%	17	17 - 36	36
Dissolved oxygen	mg L ⁻¹	3.0	>8.6	3.0
<i>Cycle</i>				
Aerobic feed	min	80	0	0
Anaerobic feed	min	0	90	80
Aeration	min	365	382 - 393	270 - 150
Settling	min	30	1.5 - 5.0	5.0
Purge	min	5	5	5

Lab-scale assessment of the granulation strategy

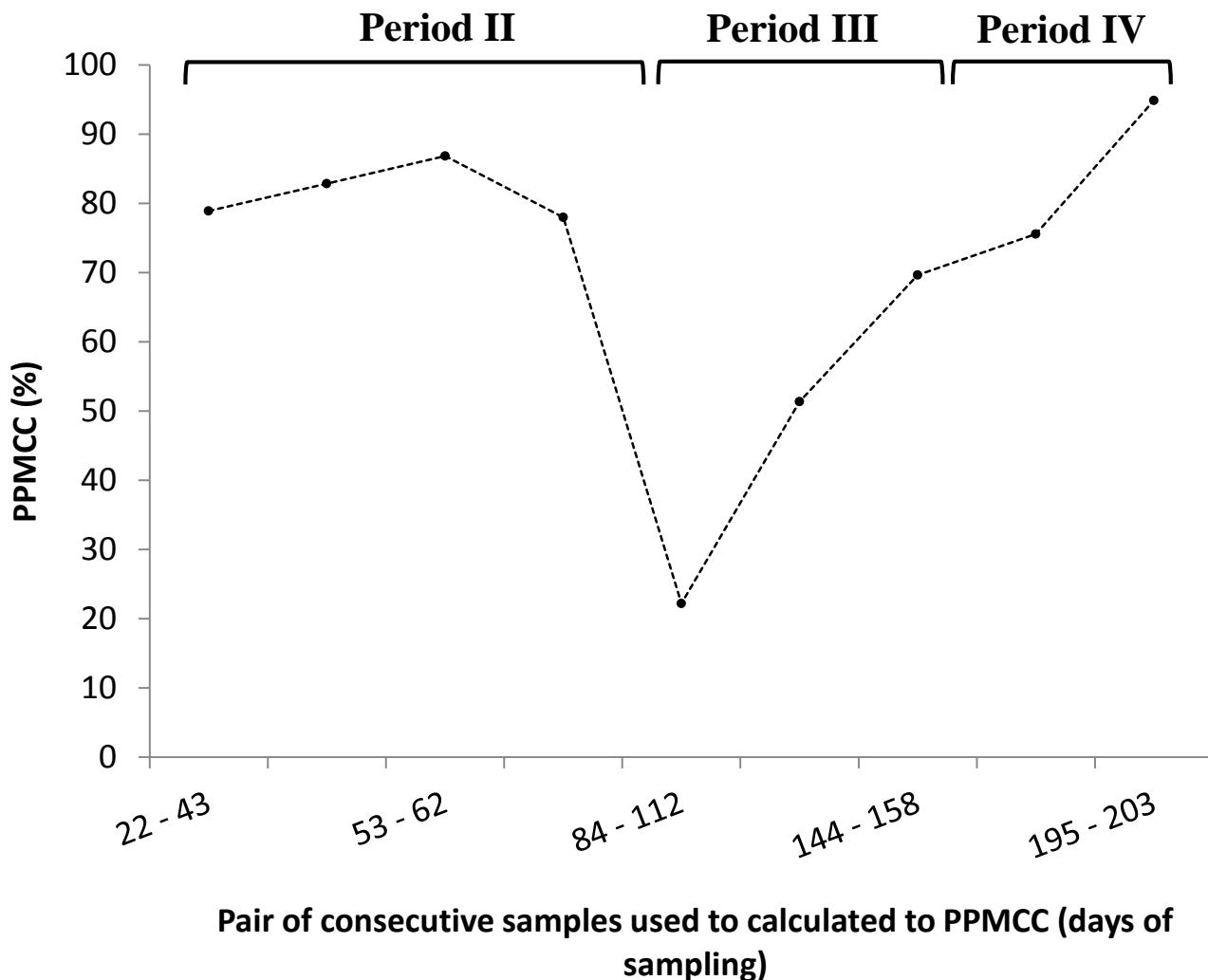


2 mm

Important switch of the microbial diversity



Important switch of the microbial diversity



Important switch of the microbial diversity

