

Supporting information

Carbon bed post-plasma to enhance the CO₂ conversion and remove O₂ from the product stream

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Supporting information includes 1) a scheme of the anode and basket; 2) SEM images for charcoal 1, before and after the gasification reactions; 3) TGA-MS under O₂ atmosphere for charcoal 1 and 2; TGA-MS under argon atmosphere for charcoal 1 4) as received, 5) after 45 s and 6) 7 minutes of reaction; 7) weight loss (TGA) for charcoal 1, before and after reaction; 8) O₂ concentration measured in the carbon bed; 9) the concentration profiles of CO₂, CO and O₂ and temperature measured in the carbon bed; Rate of the main heterogeneous reactions triggered by the carbon bed with O₂ as feed gas at 10) 1086 K and at 1502 K 11) at the beginning of the treatment and 12) after 10 minutes; 13) Rate of the main heterogeneous reactions triggered by the carbon bed with CO₂ as feed gas at 1412 K.

Figure S1

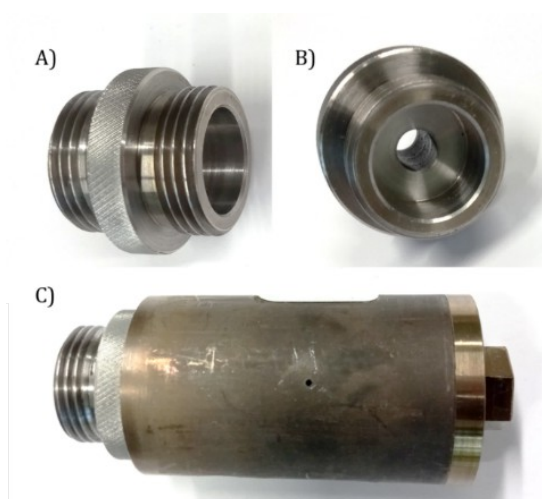


Figure S1. A. and B. Side view and front view of the anode. C. Anode and basket assembled.

Figure S2

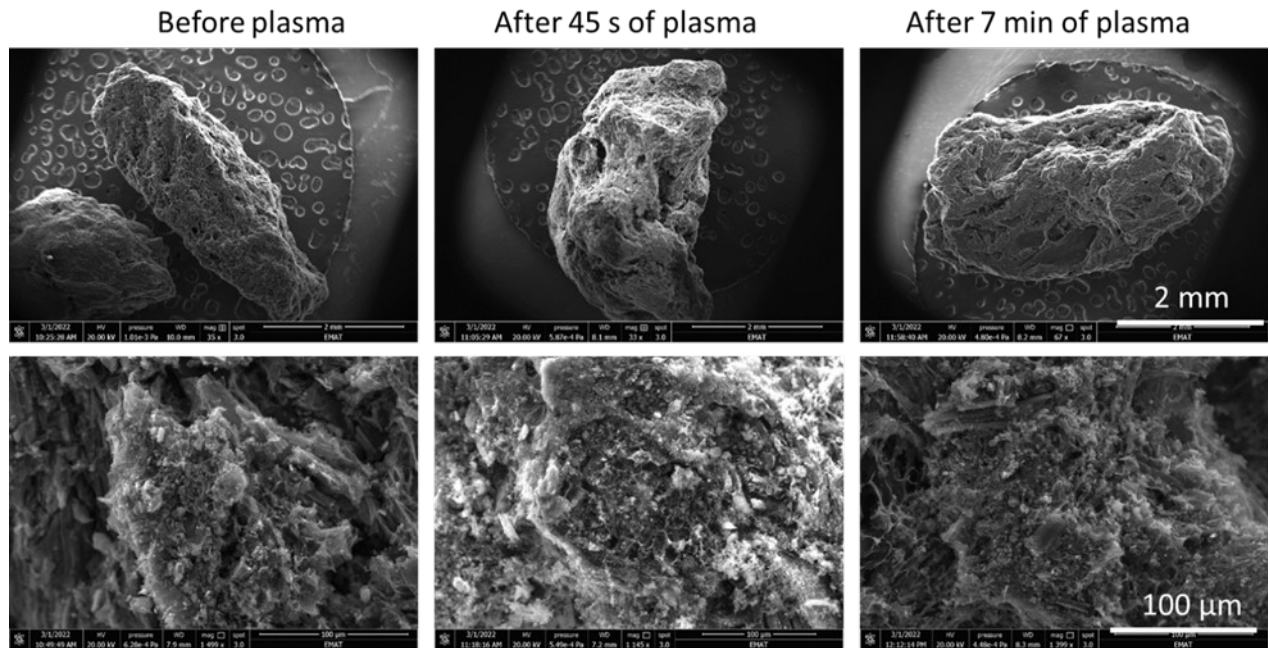


Figure S2. SEM images of charcoal 1, before and after the gasification reaction.

Figure S3

Figure S3. Partial pressure of CO₂ released from TGA-MS under O₂ atmosphere of charcoal 1 (dark blue) and charcoal 2 (light blue) and weight loss for charcoal 1 (orange dashed line) and charcoal 2 (red dashed line), as a function of the temperature and time.

Figure S4

Figure S4. TGA-MS under argon atmosphere of charcoal 1 as received.

Figure S5

Figure S5. TGA-MS of charcoal 1, top layer, after 45 s of reaction.

Figure S6

Figure S6. TGA-MS of charcoal 1, after 7 minutes of reaction.

Figure S7

Figure S7. TGA of charcoal 1, as received and after 45 s and 7 minutes of reaction.

Figure S8

Figure S8. O₂ concentration measured in real time with carbon bed, charcoal 1 (zoom in from Figure 5B in the main paper). 10L/min CO₂, SEI = 3.2 kJ.L⁻¹.

Figure S9

Figure S9. CO₂, CO and O₂ concentration profiles compared with the temperature profile obtained in the presence of the carbon bed. Charcoal 1, 10 L.min⁻¹ CO₂, SEI = 3.2 kJ.L⁻¹.

Figure S10

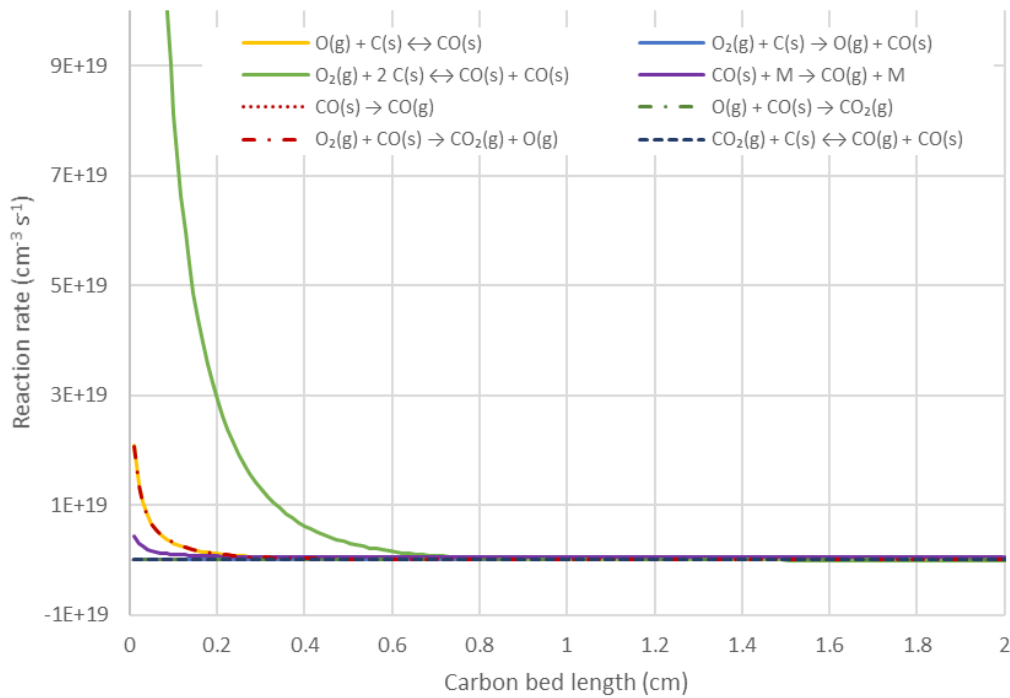


Figure S10. Rate of the main heterogeneous reactions triggered by the carbon bed at 1086 K, with O₂ as feed gas (O_{2_E}).

Figure S11

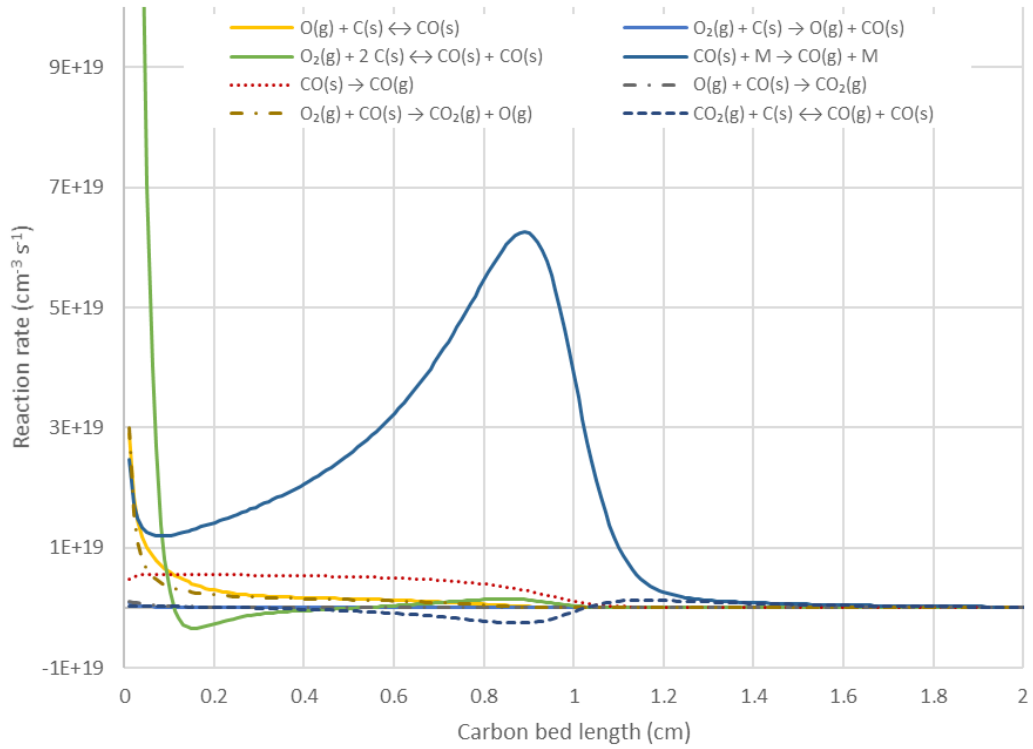


Figure S11. Rate of the main heterogeneous reactions triggered by the carbon bed at 1502 K, with O_2 as feed gas ($\text{O}_2\text{-H}$).

Figure S12

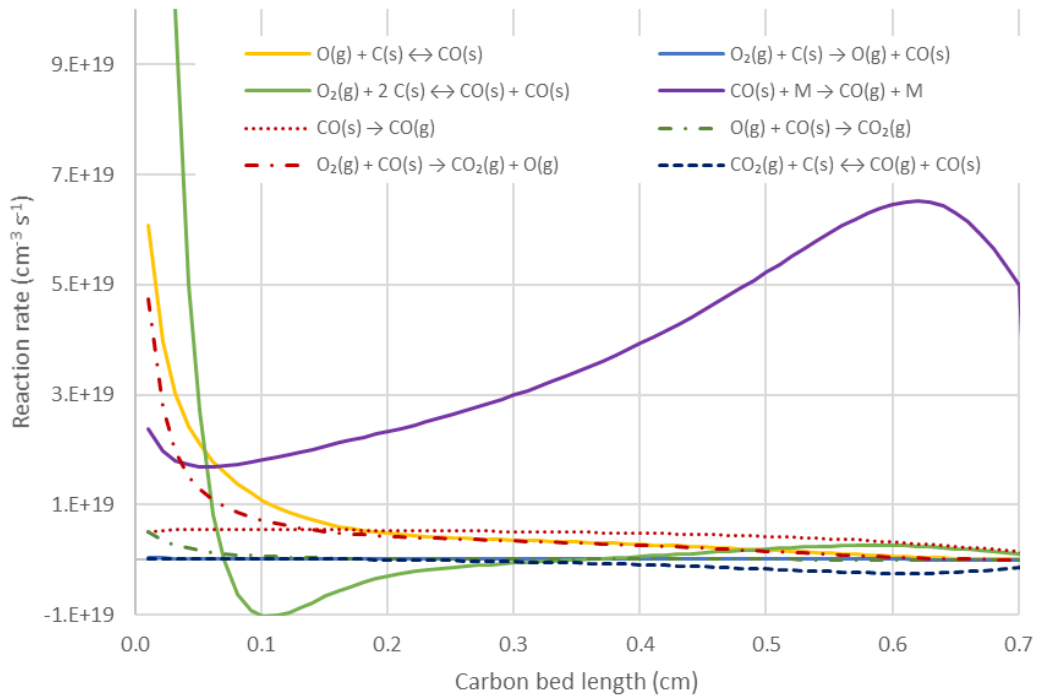


Figure S12. Rate of the main heterogeneous reactions triggered by the carbon bed at 1502 K, with O_2 as feed gas, after 10 minutes of treatment ($\text{O}_2\text{-H}_{600}$).

Figure S13

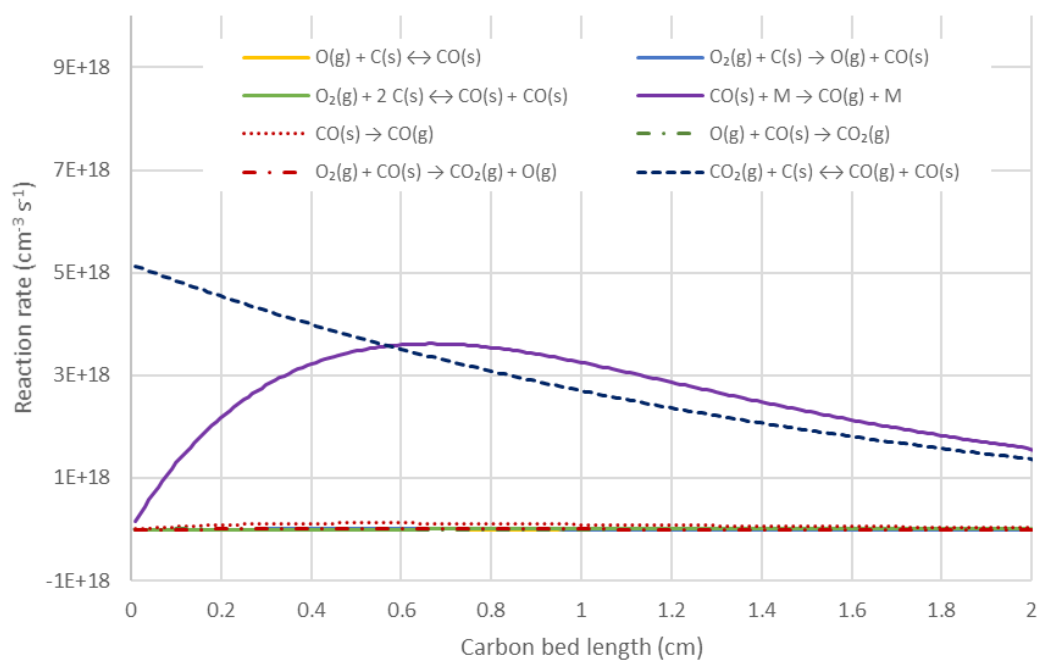


Figure S13. Rate of the main heterogeneous reactions triggered by the carbon bed at 1413 K, with CO_2 as feed gas ($\text{CO}_2\text{-H}$).

